



FENOMENOS DE TRANSPORTE EN METALURGIA

TRANSFERENCIA DE MOMENTUM

Clase 02/07

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Generalidades

- ✓ *La ec. de Navier Stokes corresponde a la ecuación general de balance de flujo de momentum y es valida para describir el comportamiento de todo tipo de flujo.*
- ✓ *Cuando se desea resolver problemas simples de flujos iso-termales en donde ρ y μ son constantes es preferible aplicar balances simples diferenciales de momentum.*
- ✓ *La ec. de Navier Stokes es utilizada en conjunto con la ec. de continuidad para simplificar su desarrollo.*
- ✓ *Ambas ecuaciones pueden ser desarrolladas vectorial o tensorialmente dependiendo de las condiciones del problema a enfrentar.*

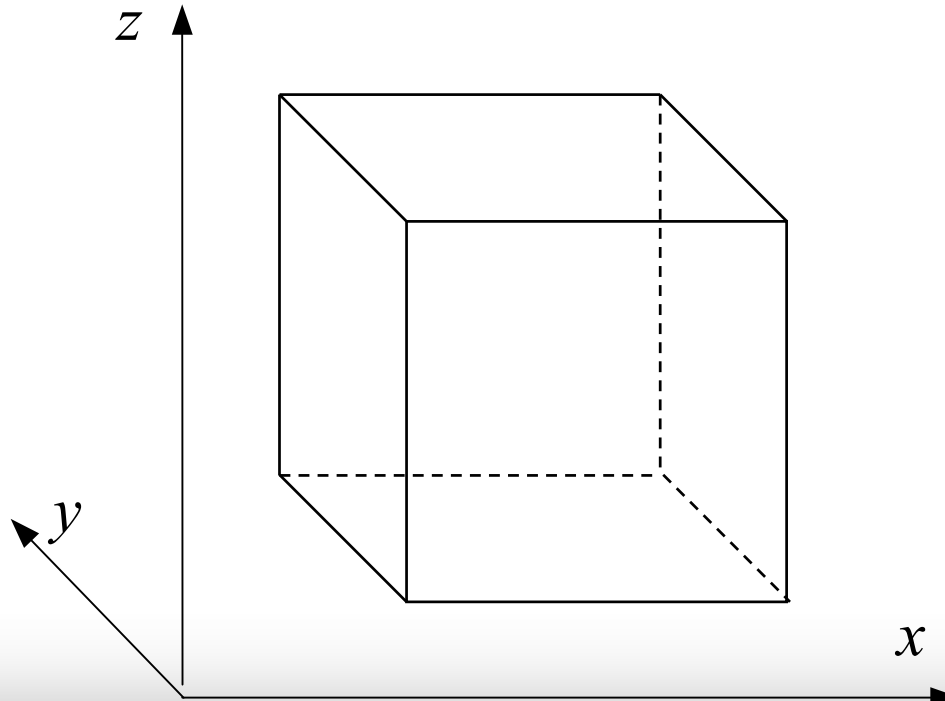


Generalidades

- ✓ *La utilización conjunta de estas ecuaciones, representan la solución matemática a problemas de flujo de fluidos, son ecuaciones complejas y no siempre entregan soluciones exactas.*
- ✓ *La ec. de continuidad se desarrolla a partir de la aplicación de la ley de conservación de masa a un elemento de volumen pequeño inmerso en un flujo.*
- ✓ *Ambas ecuaciones son validas para resolver problemas de flujo laminar y turbulento, sin embargo debido a su complejidad, se prefiere abordar estos últimos mediante modelos empíricos.*

Para desarrollar la ec. debemos aplicar la ley de conservación de masa a un elemento de volumen inmerso en un fluido en movimiento que presenta las componentes de velocidad, v_x , v_y y v_z .

$$\left(\begin{array}{c} \text{Acumulación de} \\ \text{flujo de masa} \end{array} \right) = \left(\begin{array}{c} \text{Flujo de masa} \\ \text{entrante} \end{array} \right) - \left(\begin{array}{c} \text{Flujo de masa} \\ \text{saliente} \end{array} \right)$$



El flujo de volumen del fluido que entra a través de la sección transversal perpendicular a la dirección- x es el producto de la velocidad (componente- x) y el área de la sección transversal:

$$\Delta y \Delta z v_x \Big|_x$$

El flujo másico del fluido que entra a través de la sección transversal- x perpendicular a la dirección- x es:

$$\Delta y \Delta z (\rho v_x) \Big|_x$$

El flujo másico del fluido que sale a través de la sección transversal- $x+\Delta x$ perpendicular a la dirección- x es:

$$\Delta y \Delta z (\rho v_x) \Big|_{x+\Delta x}$$

Las expresiones de flujo másico que entran y salen a través de las otras secciones transversales perpendiculares a las direcciones- y , $-z$, son análogas.

La acumulación, es la velocidad del cambio de masa en el elemento de volumen de control:

$$\Delta x \Delta y \Delta z \frac{\partial \rho}{\partial t}$$

\therefore El balance general de masa es:

$$\Delta x \Delta y \Delta z \frac{\partial \rho}{\partial t} = \Delta y \Delta z (\rho v_x|_x - \rho v_x|_{x+\Delta x}) + \dots$$

$$\dots + \Delta x \Delta z (\rho v_y|_y - \rho v_y|_{y+\Delta y}) + \Delta x \Delta y (\rho v_z|_z - \rho v_z|_{z+\Delta z})$$

Dividiendo por el volumen de control $\Delta x \Delta y \Delta z$ y haciéndolo tender a 0, se obtiene la ec. de continuidad:

$$\frac{\partial \rho}{\partial t} = - \left(\frac{\partial}{\partial x} \rho v_x + \frac{\partial}{\partial y} \rho v_y + \frac{\partial}{\partial z} \rho v_z \right)$$

Para fluidos de densidad ρ constante (mayoría de problemas de ingeniería), la ecuación de continuidad puede reducirse a la forma:

$$\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} + \frac{\partial v_z}{\partial z} = 0$$

En notación vectorial:

$$\nabla \cdot \mathbf{v} = 0$$

Para todo tipo de flujos incluidos aquellos no estacionarios, el balance general de flujo de momentum queda definido por:

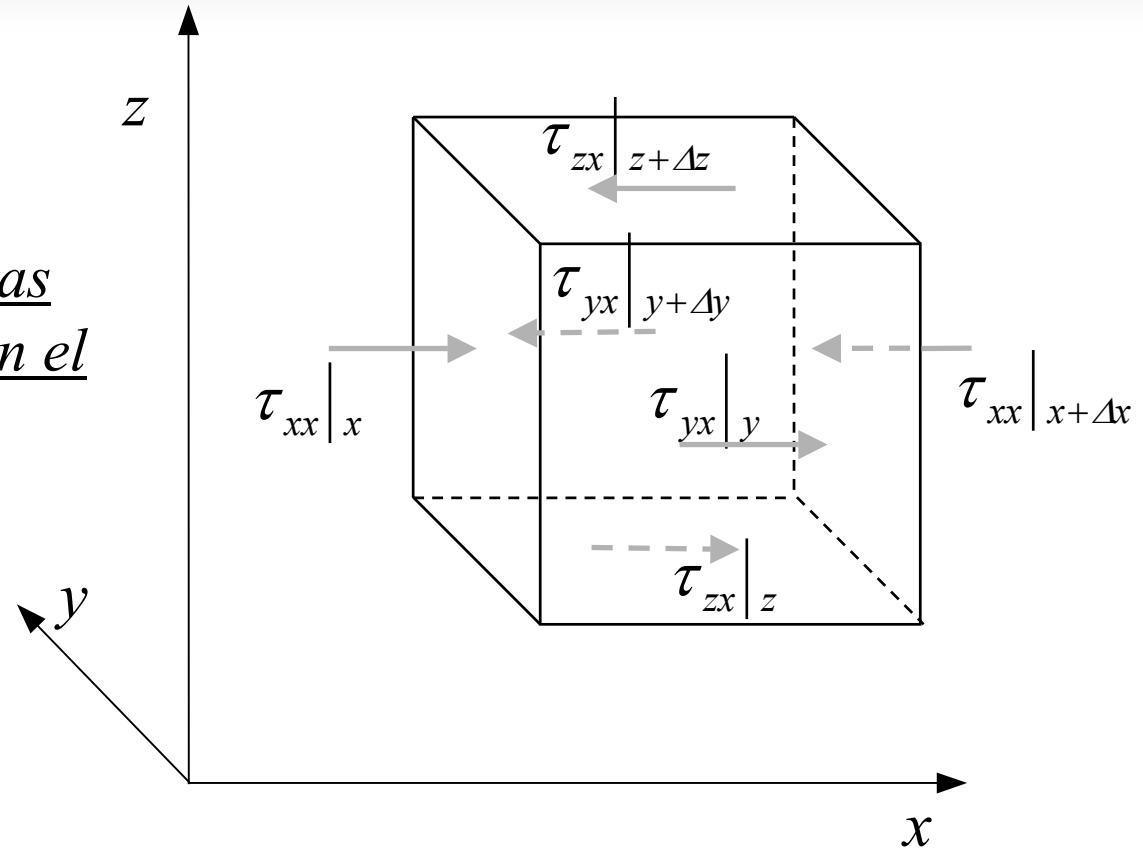
$$\left(\begin{array}{c} \text{Flujo de mom.} \\ \text{entrante} \end{array} \right) - \left(\begin{array}{c} \text{Flujo de mom.} \\ \text{saliente} \end{array} \right) + \left(\sum \vec{F} \text{ del sist.} \right) = \left(\begin{array}{c} \text{Acumulación de} \\ \text{Flujo de mom.} \end{array} \right)$$

Por simplicidad consideraremos sólo la componente-x de cada uno de los términos. Las componentes-y, -z, resultan análogas:

Debemos considerar el flujo de momentum combinado total que entra y sale por las superficies del volumen de control por efecto de la componente-x del fluido.

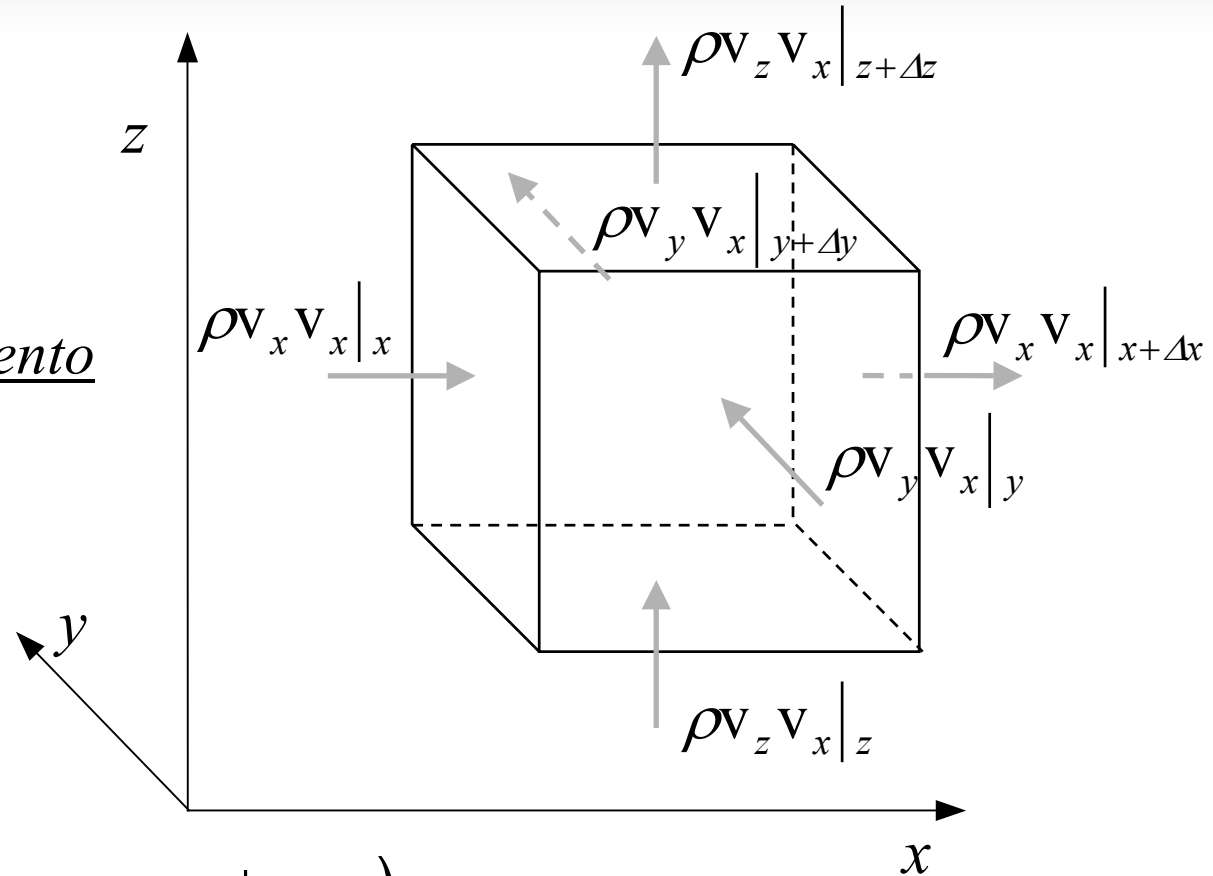
$$\phi_{ij} = \pi_{ij} + \rho v_i v_j = p + \tau_{ij} + \rho v_i v_j$$

Fuerzas viscosas causadas por el stress molecular en el volumen de control



$$\begin{aligned}
 & \Delta y \Delta z \left(\tau_{xx} \Big|_x - \tau_{xx} \Big|_{x+\Delta x} \right) + \dots \\
 & \dots + \Delta x \Delta z \left(\tau_{yx} \Big|_y - \tau_{yx} \Big|_{y+\Delta y} \right) + \dots \\
 & \dots + \Delta x \Delta y \left(\tau_{zx} \Big|_z - \tau_{zx} \Big|_{z+\Delta z} \right)
 \end{aligned}$$

Fuerzas convectivas
causadas por el movimiento
del seno del fluido
(momentum-x)



$$\begin{aligned}
 & \Delta y \Delta z \left(\rho v_x v_x \Big|_x - \rho v_x v_x \Big|_{x+\Delta x} \right) + \dots \\
 & \dots + \Delta x \Delta z \left(\rho v_y v_x \Big|_y - \rho v_y v_x \Big|_{y+\Delta y} \right) + \dots \\
 & \dots + \Delta x \Delta y \left(\rho v_z v_x \Big|_z - \rho v_z v_x \Big|_{z+\Delta z} \right)
 \end{aligned}$$

Fuerzas del sistema

En la mayoría de los casos, las fuerzas actuando sobre el sistema provienen de la presión P y de la aceleración de gravedad g por unidad de masa. En la dirección- x , estas fuerzas serán:

$$\Delta y \Delta z (P|_x - P|_{x+\Delta x})$$

$$\rho g_x \Delta x \Delta y \Delta z$$

Finalmente, la acumulación de flujo de momentum- x en el volumen de control es:

$$\Delta x \Delta y \Delta z \left(\frac{\partial}{\partial t} \rho v_x \right)$$

Dividiendo por el volumen de control $\Delta x \Delta y \Delta z$ y haciéndolo tender a 0, se obtiene la ec. de momentum de la componente-x:

$$\begin{aligned}
 \frac{\partial}{\partial t} \rho v_x &= - \left(\frac{\partial}{\partial x} \rho v_x v_x + \frac{\partial}{\partial y} \rho v_y v_x + \frac{\partial}{\partial z} \rho v_z v_x \right) - \dots \\
 \dots &- \left(\frac{\partial}{\partial x} \tau_{xx} + \frac{\partial}{\partial y} \tau_{yx} + \frac{\partial}{\partial z} \tau_{zx} \right) - \frac{\partial P}{\partial x} + \rho g_x
 \end{aligned}$$

Ecuación General de Momentum

De manera análoga se obtienen las ecs. de momentum de las componentes -y, -z:

$$\frac{\partial}{\partial t} \rho v_y = - \left(\frac{\partial}{\partial x} \rho v_x v_y + \frac{\partial}{\partial y} \rho v_y v_y + \frac{\partial}{\partial z} \rho v_z v_y \right) - \dots$$

$$\dots - \left(\frac{\partial}{\partial x} \tau_{xy} + \frac{\partial}{\partial y} \tau_{yy} + \frac{\partial}{\partial z} \tau_{zy} \right) - \frac{\partial P}{\partial y} + \rho g_y$$

$$\frac{\partial}{\partial t} \rho v_z = - \left(\frac{\partial}{\partial x} \rho v_x v_z + \frac{\partial}{\partial y} \rho v_y v_z + \frac{\partial}{\partial z} \rho v_z v_z \right) - \dots$$

$$\dots - \left(\frac{\partial}{\partial x} \tau_{xz} + \frac{\partial}{\partial y} \tau_{yz} + \frac{\partial}{\partial z} \tau_{zz} \right) - \frac{\partial P}{\partial z} + \rho g_z$$



Utilizando notación vectorial es posible resumir las ecuaciones anteriores. Representación vectorial de la velocidad másica, ρv , y de la aceleración, g , son triviales y conocidas, sin embargo, los términos $\partial P/\partial x, \partial P/\partial y, \partial P/\partial z$ representan gradientes de presión.

La presión es una cantidad escalar, pero el gradiente de presión es un vector denotado por ∇P ó bien $\text{grad } P$. \therefore

$$\nabla P = \frac{\partial}{\partial x} P + \frac{\partial}{\partial y} P + \frac{\partial}{\partial z} P$$

donde:

$$\nabla = \frac{\partial}{\partial x} + \frac{\partial}{\partial y} + \frac{\partial}{\partial z}$$



Expresión general para la ley de conservación de momentum sobre un volumen de control inmerso en un fluido en movimiento:

$$\frac{\partial}{\partial t} \rho \mathbf{v} = -(\nabla \cdot \rho \mathbf{v} \mathbf{v}) - \nabla P - (\nabla \cdot \boldsymbol{\tau}) + \rho \mathbf{g}$$

Sin embargo, necesitamos relacionar los esfuerzos de corte o componentes viscosos de esta ecuación con los gradientes de velocidad y con las propiedades del fluido para determinar las distribuciones de velocidad:

Para fluidos Newtonianos incorporamos el tensor de esfuerzos, los nueve componentes de $\boldsymbol{\tau}$, 3 relacionados con los esfuerzos normales y 6 relacionados los esfuerzos de corte.



*Esfuerzos
normales*

$$\left\{ \begin{array}{l} \tau_{xx} = -2\mu \frac{\partial v_x}{\partial x} + \frac{2}{3}\mu (\nabla \cdot \mathbf{v}) \\ \tau_{yy} = -2\mu \frac{\partial v_y}{\partial y} + \frac{2}{3}\mu (\nabla \cdot \mathbf{v}) \\ \tau_{zz} = -2\mu \frac{\partial v_z}{\partial z} + \frac{2}{3}\mu (\nabla \cdot \mathbf{v}) \end{array} \right.$$



Tensor de esfuerzos viscosos de Newton



*Esfuerzos
de corte*

$$\left\{ \begin{array}{l} \tau_{xy} = \tau_{yx} = -\mu \left(\frac{\partial v_x}{\partial y} + \frac{\partial v_y}{\partial x} \right) \\ \tau_{yz} = \tau_{zy} = -\mu \left(\frac{\partial v_y}{\partial z} + \frac{\partial v_z}{\partial y} \right) \\ \tau_{zx} = \tau_{xz} = -\mu \left(\frac{\partial v_z}{\partial x} + \frac{\partial v_x}{\partial z} \right) \end{array} \right.$$

Esta ecuación asume que tanto la densidad, ρ , como la viscosidad, μ , son constantes y \therefore :

$$\nabla \cdot \mathbf{v} = 0$$

$$\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} + \frac{\partial v_z}{\partial z} = 0$$

luego:

$$\rho \left[\frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right] = -\frac{\partial P}{\partial x} + \mu \left[\frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial z^2} \right] + \rho g_x$$

$$\rho \left[\frac{\partial v_y}{\partial t} + v_x \frac{\partial v_y}{\partial x} + v_y \frac{\partial v_y}{\partial y} + v_z \frac{\partial v_y}{\partial z} \right] = -\frac{\partial P}{\partial y} + \mu \left[\frac{\partial^2 v_y}{\partial x^2} + \frac{\partial^2 v_y}{\partial y^2} + \frac{\partial^2 v_y}{\partial z^2} \right] + \rho g_y$$

$$\rho \left[\frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right] = -\frac{\partial P}{\partial z} + \mu \left[\frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right] + \rho g_z$$

Consideremos un volumen de control de un fluido moviéndose en un espacio sin flujo másico a través de su superficie, los cambios en la componente- x de su velocidad con el tiempo y posición serán:

$$\Delta v_x = \frac{\partial v_x}{\partial t} \Delta t + \frac{\partial v_x}{\partial x} \Delta x + \frac{\partial v_x}{\partial y} \Delta y + \frac{\partial v_x}{\partial z} \Delta z$$

Además la componente- x de la aceleración esta definida como:

$$a_x = \lim_{\Delta t \rightarrow 0} \frac{\Delta v_x}{\Delta t} = \lim_{\Delta t \rightarrow 0} \left\{ \frac{\partial v_x}{\partial t} \frac{\Delta t}{\Delta t} + \frac{\partial v_x}{\partial x} \frac{\Delta x}{\Delta t} + \frac{\partial v_x}{\partial y} \frac{\Delta y}{\Delta t} + \frac{\partial v_x}{\partial z} \frac{\Delta z}{\Delta t} \right\}$$

Obteniendo:

$$a_x = \frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} = \frac{Dv_x}{Dt}$$

La ec. Corresponde a la derivada substancial vista como la aceleración sobre el volumen de control. Expresiones análogas existen para las direcciones -y, -z, representando el sistema por las correspondientes 3 derivadas substanciales y ∴:

$$\rho \frac{D\mathbf{v}}{Dt} = -\nabla P + \mu \nabla^2 \mathbf{v} + \rho \mathbf{g}$$

Ec. de Navier-Stokes, que atribuye la Ley de Newton en su forma de masa (ρ) por aceleración ($D\mathbf{v}/Dt$) igual a la suma de fuerzas, siendo estas; las fuerzas de presión (∇P), las fuerzas viscosas ($\mu \nabla^2 \mathbf{v}$) y las fuerzas de gravedad o de cuerpo ($\rho \mathbf{g}$).

Table 2.1 The continuity equation in different coordinates systems

Rectangular coordinates (x, y, z) :

$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x}(\rho v_x) + \frac{\partial}{\partial y}(\rho v_y) + \frac{\partial}{\partial z}(\rho v_z) = 0 \quad (\text{A})$$

Cylindrical coordinates (r, θ, z) :

$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r}(\rho r v_r) + \frac{1}{r} \frac{\partial}{\partial \theta}(\rho v_\theta) + \frac{\partial}{\partial z}(\rho v_z) = 0 \quad (\text{B})$$

Spherical coordinates (r, θ, ϕ) :

$$\frac{\partial \rho}{\partial t} + \frac{1}{r^2} \frac{\partial}{\partial r}(\rho r^2 v_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta}(\rho v_\theta \sin \theta) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \phi}(\rho v_\phi) = 0 \quad (\text{C})$$

*Tables 2.1-2.7 are from R. B. Bird, W. E. Stewart, and E. N. Lightfoot, *Transport Phenomena* Wiley, New York, 1960, pages 83-91. Reprinted by permission.



Table 2.2 The momentum equation in rectangular coordinates (x, y, z)

In terms of τ :

$$\begin{aligned} \text{x-component} \quad \rho \left(\frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right) = & -\frac{\partial P}{\partial x} \\ & - \left(\frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{yx}}{\partial y} + \frac{\partial \tau_{zx}}{\partial z} \right) + \rho g_x \quad (\text{A}) \end{aligned}$$

$$\begin{aligned} \text{y-component} \quad \rho \left(\frac{\partial v_y}{\partial t} + v_x \frac{\partial v_y}{\partial x} + v_y \frac{\partial v_y}{\partial y} + v_z \frac{\partial v_y}{\partial z} \right) = & -\frac{\partial P}{\partial y} \\ & - \left(\frac{\partial \tau_{xy}}{\partial x} + \frac{\partial \tau_{yy}}{\partial y} + \frac{\partial \tau_{zy}}{\partial z} \right) + \rho g_y \quad (\text{B}) \end{aligned}$$

$$\begin{aligned} \text{z-component} \quad \rho \left(\frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right) = & -\frac{\partial P}{\partial z} \\ & - \left(\frac{\partial \tau_{xz}}{\partial x} + \frac{\partial \tau_{yz}}{\partial y} + \frac{\partial \tau_{zz}}{\partial z} \right) + \rho g_z \quad (\text{C}) \end{aligned}$$



In terms of velocity gradients for a Newtonian fluid with constant ρ and μ :

$$\begin{aligned} \text{x-component} \quad \rho \left(\frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right) &= -\frac{\partial P}{\partial x} \\ &+ \mu \left(\frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial z^2} \right) + \rho g_x \end{aligned} \quad (D)$$

$$\begin{aligned} \text{y-component} \quad \rho \left(\frac{\partial v_y}{\partial t} + v_x \frac{\partial v_y}{\partial x} + v_y \frac{\partial v_y}{\partial y} + v_z \frac{\partial v_y}{\partial z} \right) &= -\frac{\partial P}{\partial y} \\ &+ \mu \left(\frac{\partial^2 v_y}{\partial x^2} + \frac{\partial^2 v_y}{\partial y^2} + \frac{\partial^2 v_y}{\partial z^2} \right) + \rho g_y \end{aligned} \quad (E)$$

$$\begin{aligned} \text{z-component} \quad \rho \left(\frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right) &= -\frac{\partial P}{\partial z} \\ &+ \mu \left(\frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right) + \rho g_z \end{aligned} \quad (F)$$



Table 2.3 The momentum equation in cylindrical coordinates (r, θ, z)

In terms of τ :

$$\begin{aligned}
 \text{r-component*} \quad \rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta^2}{r} + v_z \frac{\partial v_r}{\partial z} \right) = & -\frac{\partial P}{\partial r} \\
 & - \left(\frac{1}{r} \frac{\partial}{\partial r} (r \tau_{rr}) + \frac{1}{r} \frac{\partial \tau_{r\theta}}{\partial \theta} - \frac{\tau_{\theta\theta}}{r} + \frac{\partial \tau_{rz}}{\partial z} \right) + \rho g_r \quad \text{(A)}
 \end{aligned}$$

$$\begin{aligned}
 \theta\text{-component} \quad \rho \left(\frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_r v_\theta}{r} + v_z \frac{\partial v_\theta}{\partial z} \right) = & -\frac{1}{r} \frac{\partial P}{\partial \theta} \\
 & - \left(\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 \tau_{r\theta}) + \frac{1}{r} \frac{\partial \tau_{\theta\theta}}{\partial \theta} + \frac{\partial \tau_{\theta z}}{\partial z} \right) + \rho g_\theta \quad \text{(B)}
 \end{aligned}$$

$$\begin{aligned}
 \text{z-component} \quad \rho \left(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) = & -\frac{\partial P}{\partial z} \\
 & - \left(\frac{1}{r} \frac{\partial}{\partial r} (r \tau_{rz}) + \frac{1}{r} \frac{\partial \tau_{\theta z}}{\partial \theta} + \frac{\partial \tau_{zz}}{\partial z} \right) + \rho g_z \quad \text{(C)}
 \end{aligned}$$



In terms of velocity gradients for a Newtonian fluid with constant ρ and μ :

$$\begin{aligned}
 \text{r-component*} \quad \rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta^2}{r} + v_z \frac{\partial v_r}{\partial z} \right) &= -\frac{\partial P}{\partial r} \\
 + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r v_r) \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial^2 v_r}{\partial z^2} \right] + \rho g_r & \quad (D)
 \end{aligned}$$

$$\begin{aligned}
 \theta\text{-component} \quad \rho \left(\frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_r v_\theta}{r} + v_z \frac{\partial v_\theta}{\partial z} \right) &= -\frac{1}{r} \frac{\partial P}{\partial \theta} \\
 + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r v_\theta) \right) + \frac{1}{r^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} + \frac{\partial^2 v_\theta}{\partial z^2} \right] + \rho g_\theta & \quad (E)
 \end{aligned}$$

$$\begin{aligned}
 \text{z-component} \quad \rho \left(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) &= -\frac{\partial P}{\partial z} \\
 + \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right] + \rho g_z & \quad (F)
 \end{aligned}$$

*The term $\rho v_\theta^2 / r$ is the *centrifugal force*. It gives the effective force in the r -direction resulting from fluid motion in the θ -direction. This term arises automatically on transformation from rectangular to cylindrical coordinates; it does not have to be added on physical grounds.



Table 2.4 The momentum equation in spherical coordinates (r, θ, ϕ)

In terms of τ :

$$\begin{aligned}
 \text{r-component} \quad & \rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial v_r}{\partial \phi} - \frac{v_\theta^2 + v_\phi^2}{r} \right) \\
 & = -\frac{\partial P}{\partial r} - \left(\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 \tau_{rr}) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\tau_{r\theta} \sin \theta) \right. \\
 & \quad \left. + \frac{1}{r \sin \theta} \frac{\partial \tau_{r\phi}}{\partial \phi} - \frac{\tau_{\theta\theta} + \tau_{\phi\phi}}{r} \right) + \rho g_r
 \end{aligned} \tag{A}$$

$$\begin{aligned}
 \text{\theta-component} \quad & \rho \left(\frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial v_\theta}{\partial \phi} + \frac{v_r v_\theta}{r} - \frac{v_\phi^2 \cot \theta}{r} \right) \\
 & = -\frac{1}{r} \frac{\partial P}{\partial \theta} - \left(\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 \tau_{r\theta}) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\tau_{\theta\theta} \sin \theta) + \frac{1}{r \sin \theta} \frac{\partial \tau_{\theta\phi}}{\partial \phi} \right. \\
 & \quad \left. + \frac{\tau_{r\theta}}{r} - \frac{\cot \theta}{r} \tau_{\phi\phi} \right) + \rho g_\theta
 \end{aligned} \tag{B}$$

$$\begin{aligned}
 \text{\phi-component} \quad & \rho \left(\frac{\partial v_\phi}{\partial t} + v_r \frac{\partial v_\phi}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\phi}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial v_\phi}{\partial \phi} + \frac{v_\phi v_r}{r} + \frac{v_\theta v_\phi \cot \theta}{r} \right) \\
 & = -\frac{1}{r \sin \theta} \frac{\partial P}{\partial \phi} - \left(\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 \tau_{r\phi}) + \frac{1}{r} \frac{\partial \tau_{\theta\phi}}{\partial \theta} + \frac{1}{r \sin \theta} \frac{\partial \tau_{\phi\phi}}{\partial \phi} \right. \\
 & \quad \left. + \frac{\tau_{r\phi}}{r} + \frac{2 \cot \theta}{r} \tau_{\theta\phi} \right) + \rho g_\phi
 \end{aligned} \tag{C}$$



In terms of velocity gradients for a Newtonian fluid with constant ρ and μ :

$$\begin{aligned}
 \text{r-component} \quad & \rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial v_r}{\partial \phi} - \frac{v_\theta^2 + v_\phi^2}{r} \right) \\
 & = - \frac{\partial P}{\partial r} + \mu \left(\nabla^2 v_r - \frac{2}{r^2} v_r - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} - \frac{2}{r^2} v_\theta \cot \theta \right. \\
 & \quad \left. - \frac{2}{r^2 \sin \theta} \frac{\partial v_\phi}{\partial \phi} \right) + \rho g_r
 \end{aligned} \tag{D}$$

$$\begin{aligned}
 \text{\theta-component} \quad & \rho \left(\frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial v_\theta}{\partial \phi} + \frac{v_r v_\theta}{r} - \frac{v_\phi^2 \cot \theta}{r} \right) \\
 & = - \frac{1}{r} \frac{\partial P}{\partial \theta} + \mu \left(\nabla^2 v_\theta + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta}{r^2 \sin^2 \theta} - \frac{2 \cos \theta}{r^2 \sin^2 \theta} \frac{\partial v_\phi}{\partial \phi} \right) + \rho g_\theta
 \end{aligned} \tag{E}$$

$$\begin{aligned}
 \text{\phi-component} \quad & \rho \left(\frac{\partial v_\phi}{\partial t} + v_r \frac{\partial v_\phi}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\phi}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial v_\phi}{\partial \phi} + \frac{v_\phi v_r}{r} + \frac{v_\theta v_\phi \cot \theta}{r} \right) \\
 & = - \frac{1}{r \sin \theta} \frac{\partial P}{\partial \phi} + \mu \left(\nabla^2 v_\phi - \frac{v_\phi}{r^2 \sin^2 \theta} + \frac{2}{r^2 \sin \theta} \frac{\partial v_r}{\partial \phi} \right. \\
 & \quad \left. + \frac{2 \cos \theta}{r^2 \sin^2 \theta} \frac{\partial v_\theta}{\partial \phi} \right) + \rho g_\phi
 \end{aligned} \tag{F}$$



Table 2.5 Components of the stress tensor in rectangular coordinates (x, y, z)

$$\tau_{xx} = -\mu \left[2 \frac{\partial v_x}{\partial x} - \frac{2}{3}(\nabla \cdot \mathbf{v}) \right] \quad (\text{A})$$

$$\tau_{yy} = -\mu \left[2 \frac{\partial v_y}{\partial y} - \frac{2}{3}(\nabla \cdot \mathbf{v}) \right] \quad (\text{B})$$

$$\tau_{zz} = -\mu \left[2 \frac{\partial v_z}{\partial z} - \frac{2}{3}(\nabla \cdot \mathbf{v}) \right] \quad (\text{C})$$

$$\tau_{xy} = \tau_{yx} = -\mu \left[\frac{\partial v_x}{\partial y} + \frac{\partial v_y}{\partial x} \right] \quad (\text{D})$$

$$\tau_{yz} = \tau_{zy} = -\mu \left[\frac{\partial v_y}{\partial z} + \frac{\partial v_z}{\partial y} \right] \quad (\text{E})$$

$$\tau_{zx} = \tau_{xz} = -\mu \left[\frac{\partial v_z}{\partial x} + \frac{\partial v_x}{\partial z} \right] \quad (\text{F})$$

$$(\nabla \cdot \mathbf{v}) = \frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} + \frac{\partial v_z}{\partial z} \quad (\text{G})$$



Table 2.6 Components of the stress tensor in cylindrical coordinates (r, θ, z)

$$\tau_{rr} = -\mu \left[2 \frac{\partial v_r}{\partial r} - \frac{2}{3} (\nabla \cdot \mathbf{v}) \right] \quad (\text{A})$$

$$\tau_{\theta\theta} = -\mu \left[2 \left(\frac{1}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_r}{r} \right) - \frac{2}{3} (\nabla \cdot \mathbf{v}) \right] \quad (\text{B})$$

$$\tau_{zz} = -\mu \left[2 \frac{\partial v_z}{\partial z} - \frac{2}{3} (\nabla \cdot \mathbf{v}) \right] \quad (\text{C})$$

$$\tau_{r\theta} = \tau_{\theta r} = -\mu \left[r \frac{\partial}{\partial r} \left(\frac{v_\theta}{r} \right) + \frac{1}{r} \frac{\partial v_r}{\partial \theta} \right] \quad (\text{D})$$

$$\tau_{\theta z} = \tau_{z\theta} = -\mu \left[\frac{\partial v_\theta}{\partial z} + \frac{1}{r} \frac{\partial v_z}{\partial \theta} \right] \quad (\text{E})$$

$$\tau_{zr} = \tau_{rz} = -\mu \left[\frac{\partial v_z}{\partial r} + \frac{\partial v_r}{\partial z} \right] \quad (\text{F})$$

$$(\nabla \cdot \mathbf{v}) = \frac{1}{r} \frac{\partial}{\partial r} (r v_r) + \frac{1}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial v_z}{\partial z} \quad (\text{G})$$



Table 2.7 Components of the stress tensor in spherical coordinates (r, θ, ϕ)

$$\tau_{rr} = -\mu \left[2 \frac{\partial v_r}{\partial r} - \frac{2}{3}(\nabla \cdot \mathbf{v}) \right] \quad (A)$$

$$\tau_{\theta\theta} = -\mu \left[2 \left(\frac{1}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_r}{r} \right) - \frac{2}{3}(\nabla \cdot \mathbf{v}) \right] \quad (B)$$

$$\tau_{\phi\phi} = -\mu \left[2 \left(\frac{1}{r \sin \theta} \frac{\partial v_\phi}{\partial \phi} + \frac{v_r}{r} + \frac{v_\theta \cot \theta}{r} \right) - \frac{2}{3}(\nabla \cdot \mathbf{v}) \right] \quad (C)$$

$$\tau_{r\theta} = \tau_{\theta r} = -\mu \left[r \frac{\partial}{\partial r} \left(\frac{v_\theta}{r} \right) + \frac{1}{r} \frac{\partial v_r}{\partial \theta} \right] \quad (D)$$

$$\tau_{\theta\phi} = \tau_{\phi\theta} = -\mu \left[\frac{\sin \theta}{r} \frac{\partial}{\partial \theta} \left(\frac{v_\phi}{\sin \theta} \right) + \frac{1}{r \sin \theta} \frac{\partial v_\theta}{\partial \phi} \right] \quad (E)$$

$$\tau_{\phi r} = \tau_{r\phi} = -\mu \left[\frac{1}{r \sin \theta} \frac{\partial v_r}{\partial \phi} + r \frac{\partial}{\partial r} \left(\frac{v_\phi}{r} \right) \right] \quad (F)$$

$$(\nabla \cdot \mathbf{v}) = \frac{1}{r^2} \frac{\partial}{\partial r} (r^2 v_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (v_\theta \sin \theta) + \frac{1}{r \sin \theta} \frac{\partial v_\phi}{\partial \phi} \quad (G)$$